

# Effect of carboxymethylcellulose on colloidal properties of calcite suspensions in drilling fluids

Keila Regina Santana Fagundes<sup>1</sup>, Railson Carlos da Souza Luz<sup>1</sup>, Fabio Pereira Fagundes<sup>2</sup>  
and Rosângela de Carvalho Balaban<sup>1\*</sup>

<sup>1</sup>Laboratório de Pesquisa em Petróleo – LAPET, Instituto de Química – IQ, Centro de Ciências Exatas e da Terra – CCET, Universidade Federal do Rio Grande do Norte – UFRN, Natal, RN, Brasil

<sup>2</sup>Universidade Potiguar – UnP, Natal, RN, Brasil

\*rosangelabalaban@hotmail.com

## Abstract

Drilling fluids are multicomponent systems used to aid the removal of cuttings from a borehole, and subject to a number of requirements to ensure a safe drilling operation. One of the most important is to form a low permeability cake on the walls of the hole penetrated by the bit, to avoid excessive filtrate loss. To that end, carboxymethylcellulose (CMC) associated with calcite ( $\text{CaCO}_3$ ) can be used. In this paper, the effect of carboxymethylcellulose on the colloidal properties of calcite suspensions in brine was systematically evaluated by rheological properties, filtrate volume and zeta potential. Higher viscosity fluids, lower filtrate loss and less negative zeta potential were obtained using small calcite particles with wide size distribution and CMC with high average molecular weight (Mw) and low average degree of substitution (DS), highlighting the importance of effective interactions between CMC and calcite to improve drilling fluid properties.

**Keywords:** calcite,  $\text{CaCO}_3$ , CMC, drilling fluids, filtrate loss.

## 1. Introduction

Carboxymethylcellulose (CMC) is one of the most important derivatives of cellulose, primarily due to its versatility as thickener, binding agent, emulsifier and stabilizer. The presence of  $-\text{CH}_2-\text{COO}^-\text{Na}^+$  substituent groups on the cellulose backbone is responsible for higher solubility in aqueous media<sup>[1]</sup>. Polymer concentration<sup>[2]</sup>, salt content<sup>[3,4]</sup>, pH<sup>[5]</sup>, the presence of surfactant<sup>[6]</sup>, molecular structure<sup>[7]</sup>, Mw<sup>[8]</sup> and DS<sup>[9]</sup> exert important effects on CMC solution properties. This polysaccharide has been used in a wide range of applications in foods<sup>[10]</sup>, pharmaceutical products<sup>[11]</sup>, biomaterials<sup>[12]</sup>, cosmetics and electronic devices<sup>[13]</sup>, as well as in many oilfield operations, including drilling fluids<sup>[14,15]</sup>.

In most water-based drilling fluids, CMC is commonly used in association with calcite (calcium carbonate,  $\text{CaCO}_3$ ) particles to reduce fluid loss to the surrounding formation<sup>[16]</sup>. However, another important function of water soluble polymers is to provide rheological properties capable of maintaining the cuttings in suspension during drilling operations. As such, it is essential to correlate the polymer chemical structure (DS, Mw and distribution of substituent) with the physical-chemical properties of  $\text{CaCO}_3$  suspensions, in order to obtain the best result at the lowest cost.

Proper selection of CMC and  $\text{CaCO}_3$  can minimize fluid filtration across the wellbore, when a thin low-permeability filter cake is formed. According to the literature, CMC adsorption onto solid substrates is strongly dependent on adsorption kinetics, the pH of the medium and apparent hydrodynamic thickness<sup>[17]</sup>. Moreover, it also depends on the Mw and DS of CMC<sup>[18]</sup>. Caraschi and Campana<sup>[1]</sup> investigated

the influence of DS of CMC and substituent distribution profile on equilibrium properties in an aqueous medium. It was observed that the stability of aggregates is strongly influenced by the nature of group interactions ( $-\text{COOH}$  and  $-\text{OH}$ ), reconstituted bonds and electrostatic repulsions between the charged groups ( $\text{COO}^-$ ). Backfolk et al.<sup>[16]</sup> showed the adsorption and association mechanisms for CMC and  $\text{CaCO}_3$  suspensions through adsorption isotherms. They concluded that the interactions between CMC and  $\text{CaCO}_3$  are related to the amount of Lewis acid sites on  $\text{CaCO}_3$ , leading to the formation of  $\text{CMC}\cdot\text{Ca}^{2+}$  complexes. Laskowski et al.<sup>[19]</sup> investigated polysaccharide adsorption onto mineral solid surfaces. The interactions were dependent on the basic/acid features of the hydroxylated metallic sites, which are anchored to the mineral surface. Moreover, the authors reported that hydroxyl and carboxylate groups on CMC have a significant impact on how this polysaccharide adsorbs at the mineral/aqueous solution interface. Some researchers have proposed that the mechanisms responsible for polymer adsorption onto mineral surfaces include hydrophobic interaction<sup>[20]</sup>, hydrogen bonding<sup>[21,22]</sup>, as well as chemical and electrostatic interactions<sup>[23]</sup>.

In the context of complex multicomponent drilling fluids, the adsorption mechanisms of CMC onto  $\text{CaCO}_3$ , as well as the corresponding effects on fluid properties, have not been clearly elucidated. As such, the aim of this paper is to evaluate the influence of the DS and Mw of CMC on the colloidal properties of  $\text{CaCO}_3$  suspensions, through rheological properties, filtrate loss and zeta potential.

## 2. Materials and Methods

### 2.1 Materials

The following products were donated by PETROBRAS S.A.: xanthan gum, sodium chloride and calcium carbonate (calcite) of different particle sizes. CMC sodium salt, with a nominal DS/Mw of 0.7 /  $2.5 \times 10^5$  g/mol, 1.2 /  $2.5 \times 10^5$  g/mol and 0.7/0.9 x  $10^5$  g/mol were purchased from SIGMAALDRICH.

### 2.2 Characterization of CaCO<sub>3</sub>

The average particle diameter and particle size distribution curve for CaCO<sub>3</sub> (calcium carbonate, calcite) were determined by means of laser diffractometry through a CILAS 1064 laser particle analyzer. Analysis was carried out by dispersion of calcium carbonate in water, at 25 °C over the range from 0.04 to 500 μm. The data for CaCO<sub>3</sub> particle sizes were presented by the cumulative distribution as a function of particle size.

### 2.3 Fluid preparation

Xanthan gum (4.3 g/L) was used as rheological modifier in all formulations, and solubilized in 350 mL of 57 g/L sodium chloride aqueous solution for 24 hours, under constant stirring. Next, CMC and calcium carbonate were added to the polymer solution using a Hamilton Beach mixer, at 18,000 rpm. CMC and calcium carbonate were added separately and the mixing time for each product was 10 minutes. Twelve formulations were prepared and evaluated in regard to rheological behavior and filtrate volume. Table 1 shows the formulations studied.

### 2.4 Viscosity tests

A FANN model 35 A rotational viscometer was used to measure the viscosity of the colloidal suspensions. Its design includes a R1 Rotor sleeve, B1 Bob, F1 Torsion Spring, and a stainless steel sample cup for testing according to American Petroleum Institute Recommended Practice for Field Testing Water Based Drilling Fluids, API RP 13B-1/ISO 10414-1 Specification<sup>[24]</sup>. Rheological analysis of each fluid was carried out under six different shear rates (5, 10, 170, 340, 511, 1022 s<sup>-1</sup>), at 25 °C. All the experiments were carried out in triplicate.

### 2.5 Filtration properties

The filterability tests were performed in triplicate with a Whatman paper filter (Number 50), in a stainless-steel filtration cell under constant pressure of 100 psi, at 25 °C, for 30 minutes. This procedure was used to replicate the

testing conditions of API fluid –loss testing<sup>[24]</sup>. Error bars represented the standard error of the mean.

Both rheological and filtration characterization followed the recommendations of the American Petroleum Institute - RP 13B<sup>[24]</sup>.

### 2.6 Zeta potential

Zeta potential (ζ) was determined in a Zeta Potential Analyzer (Brookhaven, New York, NY, USA). Electrophoretic mobilities of particles were measured by the analyzer and converted to zeta potential using the Smoluchowski Equation. The experiments were performed at 25 °C with an equilibrium time of 24 hours for formulations F4 to F12. However, to better understand the interactions between calcium carbonate and CMC, neither xanthan gum nor NaCl was added. The suspensions were prepared by previous solubilization of CMC (8.5 g/L) in distilled water for 12 hours followed by addition of calcium carbonate (57 g/L), with continue stirring for more 12 hours. ζ values were reported with an experimental error of less than 5% (after 10 runs).

## 3. Results and Discussion

### 3.1 Influence of CMC chemical structure and CaCO<sub>3</sub> particle size on rheological properties

Figure 1 shows that rheological properties depend strongly on the composition of the fluids. The fit of the power law model (Equation 1) to the rheological data was very good, with correlation coefficients ( $R^2$ ) close to 1 (results not shown). The behavior index ( $n$ ) indicated typical pseudoplastic fluid values in the 0.47 to 0.57 range, and the consistency index varied from 346 Pa.s<sup>n</sup> (F3) to 1399 Pa.s<sup>n</sup> (F5).

$$\tau = K \left( \dot{\gamma} \right)^n \quad (1)$$

where: τ = Shear stress (Pa);  $\dot{\gamma}$  = Shear rate (s<sup>-1</sup>); K = Consistency index (Pa.s<sup>n</sup>); n = Behavioral index.

#### 3.1.1 Effect of Mw and DS of carboxymethylcellulose

Figure 2 shows the viscosity curves of F1 to F3. A significant decrease in viscosity and in consistency index (data not shown) was observed from F1 to F3. The rheological properties were greater for fluid F1 containing CMC with a higher Mw (Mw =  $2.5 \times 10^5$  g/mol) and lower DS (DS = 0.7). With an increase in Mw, the polymer hydrodynamic volume also rises, leading to higher viscosity. On the other hand, an

**Table 1.** Composition of colloidal suspensions.

Additive (g/L)	Formulations											
	F1	F2	F3	F4	F5	F6	F7	F8	F9	F10	F11	F12
Xanthan gum	4.3	4.3	4.3	4.3	4.3	4.3	4.3	4.3	4.3	4.3	4.3	4.3
CMC Mw=2.5 x 10 <sup>5</sup> ; DS=0.7	8.5			8.5	8.5	8.5						
CMC Mw=2.5 x 10 <sup>5</sup> ; DS=1.2		8.5					8.5	8.5	8.5			
CMC Mw=0.9 x 10 <sup>5</sup> ; DS=0.7			8.5							8.5	8.5	8.5
CaCO <sub>3</sub> A				57			57			57		
CaCO <sub>3</sub> B					57			57			57	
CaCO <sub>3</sub> C						57			57			57
NaCl	57	57	57	57	57	57	57	57	57	57	57	57

increase in DS can reduce CMC solubility in brine, thereby reducing viscosity. An increase in DS typically causes a more homogeneous distribution of carboxylate in the polymer chains<sup>[1]</sup>. Thus, immediate interactions may occur between salt and the polymer carboxylate groups, effectively shielding the anionic charge and inhibiting hydrogen bonds between the anionic sites and water molecules, diminishing polymer solubility in water.

### 3.1.2 Effect of CaCO<sub>3</sub> particle size

The viscosity of non-Newtonian fluids is affected by the characteristics of the dispersed solid phase, such as particle shape, concentration and dimension, solid/liquid phase interactions, nature of the surface, particle size distribution, etc<sup>[25]</sup>. Particle size distribution, uniformity factor and specific surface area are important physical parameters affecting fluids rheological and filtration behavior. It is clear that narrow and wide size distributions have different influences upon CaCO<sub>3</sub> particles properties. A wider particle size distribution increases packing density and decreases aqueous medium demand, while a narrower particle size distribution gives higher hydration rates for equal specific surface area. It is obvious that as the particle size increases the surface area decreases. Likewise, CMC Mw and DS influence directly the degree of calcium carbonate particle flocculation.

As illustrated in Figures 3 to 5, after the addition of different samples of calcium carbonate to the fluids, almost all formulations experienced an increase in rheological properties (F4-F5-F6, compared to F1; F7-F8-F9, compared to F2 and F10-F11-F12, compared to F3).

This effect might be explained by polyelectrolyte adsorption onto the calcium carbonate surface, which is responsible for the increase in apparent particle volume, as well as higher mineral stability in the medium. On the other hand, the presence of a low number of small calcium carbonate particles can act as a lubricant, improving large particle rotation (smaller particles are interspersed between larger particles), leading to a reduction in viscosity<sup>[25,26]</sup>. This last effect could explain the results of formulation F12 (Figure 5), in which the CMC with the smallest Mw was used. In F12, viscosity declined from 250 to 200 cP at a shear rate of 10 s<sup>-1</sup>. However, unlike the rheological behavior exhibited by F12, the other formulations show no decrease in viscosity in the presence of small calcium carbonate particles. This effect was likely mitigated by the strong contribution of CMC Mw and DS that altered the particles' attractive forces, responsible for controlling the state of dispersion and rheological properties of the fluids.

Table 2 shows the particle size of the CaCO<sub>3</sub> used. The calcium carbonate samples exhibited a particle size in the range of 0.87 to 17.88 μm, 1.39 to 22.06 μm and 1.92 to 32.65 μm for calcium carbonate A, B and C, respectively, with mean particle sizes of 7.64 μm, 12.27 μm and 18.61 μm, for A, B and C, respectively. These values are in agreement with the manufacturer's data. In addition, calcium carbonate A showed the lowest average diameter and largest particle diameter distribution, which means significant amounts of different particle sizes, whereas calcium carbonate B and C displayed the narrowest diameter distribution.

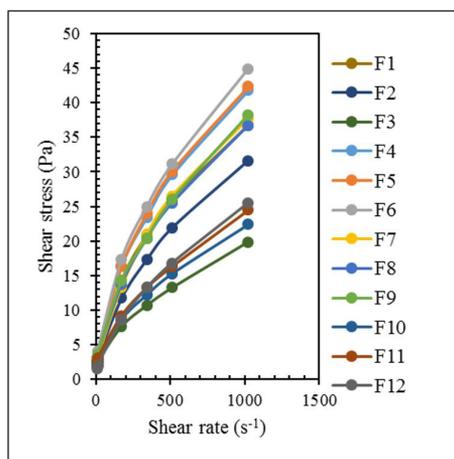


Figure 1. Flow curves of the colloidal suspensions described in Table 1, from shear rate 5 to 1022 s<sup>-1</sup>, at 25 °C.

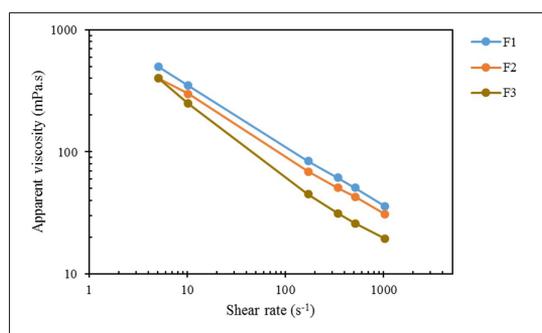


Figure 2. Viscosity curves for F1, F2 and F3 colloidal suspensions described in Table 1, from shear rate 5 to 1022 s<sup>-1</sup>, at 25 °C. F = Formulation.

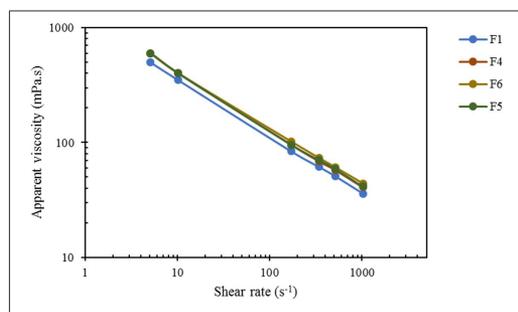
Table 2. Particle size characterization of CaCO<sub>3</sub> A; B and C.

	Average diameter (μm)	Diameter at 10% (μm)	Diameter at 50% (μm)	Diameter at 90% (μm)
CaCO <sub>3</sub> A	7.64	0.87	5.56	17.88
CaCO <sub>3</sub> B	12.27	1.39	12.40	22.06
CaCO <sub>3</sub> C	18.61	1.92	18.77	32.65

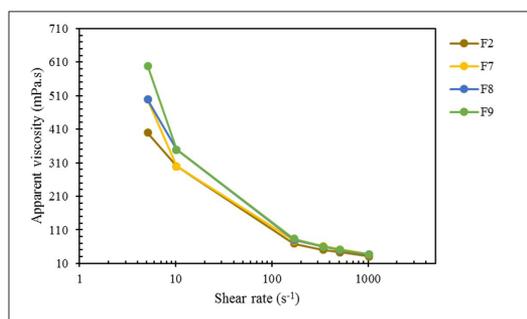
CaCO<sub>3</sub> C was the carbonate sample that contributed least to the increase in the consistency index. The effect on the flux behavior of colloidal suspensions was more marked in the viscosity results obtained when CMC with the lowest Mw was used (Figure 5), especially at low shear rates. On the other hand, the rheological properties were very similar in the formulations in which CaCO<sub>3</sub> A and CaCO<sub>3</sub> B were used. This means that an increase in CaCO<sub>3</sub> granulometry leads to fewer interactions between colloidal particles.

### 3.2 Influence of CMC chemical structure and CaCO<sub>3</sub> particle size on filtrate loss

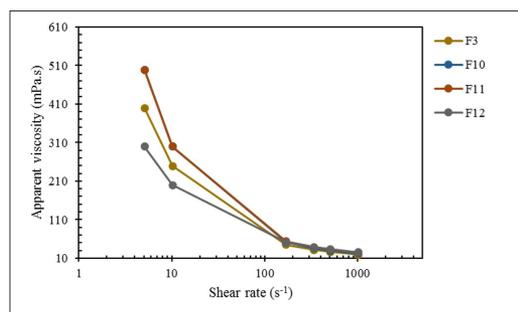
Figure 6 summarizes the influence of CMC Mw, DS and calcite granulometry on the filtrate volume of colloidal calcite suspensions.



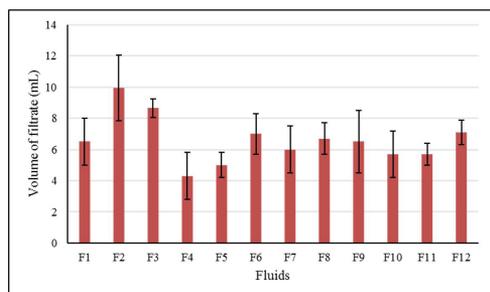
**Figure 3.** Viscosity curves for F1, F4, F5 and F6 colloidal suspensions described in Table 1, from shear rate 5 to 1022 s<sup>-1</sup>, at 25 °C. F = Formulation.



**Figure 4.** Viscosity curves for F2, F7, F8 and F9 colloidal suspensions described in Table 1, from shear rate 5 to 1022 s<sup>-1</sup>, at 25 °C. F = Formulation.



**Figure 5.** Viscosity curves for F3, F10, F11 and F12 colloidal suspensions described in Table 1, from shear rate 5 to 1022 s<sup>-1</sup>, at 25 °C. F = Formulation.



**Figure 6.** Filtrate volume of colloidal calcite suspensions, at constant pressure of 100 psi, 25 °C, for 30 min.

### 3.2.1 Effect of CMC

CMC is a water soluble organic colloid. As such, small amounts of CMC can significantly enhance water viscosity. On the other hand, filtrate volume decreases with an increase in filtrate viscosity. Another important parameter in the filtration process is the permeability of the cake formed on the surface of the filter paper. The filtrate volume decreases when filter cake permeability declines<sup>[27]</sup>. Among F1, F2 and F3 formulations, F1 showed the highest viscosity (Figure 2) and lowest filtrate volume (Figure 6) corroborating, thus, with the equation showed by Darley and Gray<sup>[27]</sup>, which evidences that the decrease of viscosity leads to an enhancement of filtrate volume. Besides, a small difference was observed between the filtrate volume of F2 and F3. There seems to be a critical polymer hydrodynamic volume that depends on CMC Mw and DS, above which the filtrate volume decreases as a response to filtrate viscosity and filter cake permeability. In the presence of salt, the effect of increasing DS is similar to that of decreasing Mw, due to the enhanced polymer collapse at a high DS.

### 3.2.2 Effect of the interaction between CMC and calcium carbonate

The dispersion of calcium carbonate is important for its surface charge and colloidal properties as well as for its interaction with polymers<sup>[16]</sup>. The presence of water-soluble polysaccharides promotes interactions with calcium carbonate that reinforce the filter cake formed during filtration and provides the desired rheological properties over large temperature ranges. It has been reported that the calcium carbonate isoelectric point (iep) should lie within the range of pH 8.0-9.5<sup>[28]</sup>. CMC is in free acid form at pH 3.5, and the acid groups are ionized (negatively charged) at about pH 7.0. This suggests that CMC may shift the CaCO<sub>3</sub> iep in solution, affecting charge development at the interface. This agrees with findings by Wang and Somasundaran<sup>[29]</sup>, which showed that CMC was responsible for the decreased zeta potential of talc with a rise in the iep from pH 2.5 to pH 3.5. This evidence suggests that electrostatic interactions play an important role in the adsorption process of CMC onto CaCO<sub>3</sub> and, consequently, in filtrate control. Figure 6 shows that CMC is responsible for the significant influence on filtrate control in association with calcium carbonate. The affinity of CMC molecules with dispersed calcium carbonate particles depends on the available Ca<sup>2+</sup> surface sites for polymer adsorption. It should be noted that not only polymer and CaCO<sub>3</sub> structure influence adsorption kinetics, but also the ionic strength of the medium. Several investigators<sup>[30]</sup> have reported that the adsorption of smaller CMC chains prevails at low salt concentrations (for example: 0.01M) due to their faster diffusion. In other words, these smaller polyelectrolytes create an electrostatic barrier that opposes the arrival of larger molecules<sup>[29]</sup>. However, in our case, a salt concentration of 1 M was used in all formulations. The lowest filtrate volume values (F4-F5) were mainly associated with the highest CMC Mw (2.5 x 10<sup>5</sup> g/mol). The electrostatic barrier collapse caused by “salt screening” causes the larger charged macromolecules to reach the calcium carbonate surface<sup>[16]</sup>. Moreover, it is reasonable to assume that the greater the interactions between CMC and Lewis acid sites on the calcium carbonate for the formation of CMC-Ca<sup>2+</sup> complexes, the faster the adsorption process

**Table 3.** Zeta potential of CaCO<sub>3</sub>/CMC colloidal suspensions.

Additive	Concentration (g/L)								
CMC Mw=2.5 x 10 <sup>5</sup> ; DS=0.7	8.5	8.5	8.5						
CMC Mw=2.5 x 10 <sup>5</sup> ; DS=1.2				8.5	8.5	8.5			
CMC Mw=0.9 x 10 <sup>5</sup> ; DS=0.7							8.5	8.5	8.5
CaCO <sub>3</sub> A	57			57			57		
CaCO <sub>3</sub> B		57			57			57	
CaCO <sub>3</sub> C			57			57			57
ζ (mV)	-11.95	-4.82	-13.01	-19.02	-34.00	-36.09	-41.20	-14.51	+27.12

and, consequently, the lower the filtrate volume. This effect contributed to the decline in filtrate volume for F7-F8-F9, compared to F2, due to the higher DS of CMC.

### 3.2.3 Effect of CaCO<sub>3</sub> particle size

Understanding the filtration mechanism that allows the establishment of an association between calcium carbonate particle size and the filtration properties of water-based drilling fluids is a daunting challenge in elucidating the problems related to fluid loss in wellbores. According to the results obtained (Figure 6), the formulations with the largest average calcium carbonate particle size (18.61 μm) exhibited the highest filtrate volume, caused by formation of a higher permeability filter cake. At the beginning of filtration, the colloidal suspension invades the porous medium (spurt loss). The suspended solids attempt to flow with the liquid stream, but a fraction of these particles bridge the pores and begin to build a filter cake. Finer particles fill the interstices left by the bridging particles and ultimately form such a tight matrix that only liquid (filtrate) can penetrate. Once this filter cake is established, the flow rate of fluid into the porous medium is dictated by the permeability of the cake<sup>27</sup>. Thus, in addition to average particle size, another important parameter is particle size distribution. Table 2 shows that CaCO<sub>3</sub> A has the widest diameter distribution curve, with particles of different sizes, while CaCO<sub>3</sub> B and CaCO<sub>3</sub> C have narrower curves. The results in Figure 6 demonstrate that CaCO<sub>3</sub> A, with the smallest average diameter particle and widest diameter distribution curve, was more effective in controlling filtrate volume, producing a low-permeability filter cake.

### 3.3 Influence of CMC chemical structure and CaCO<sub>3</sub> particle size on zeta potential

Zeta potential (ζ) provides an indirect measurement of surface charge density and is a relative indicator of system stability. The electrical properties of the calcium carbonate/CMC interface were investigated in order to elucidate the mechanisms that dictate charging behavior at the solid-liquid interface and, consequently, improve understanding of the electrochemical double layer (EDL) in the shear plane between the CaCO<sub>3</sub> particle surface and counterions near the surface and surrounding polymeric fluid. Table 3 shows the zeta potential of the colloidal suspensions as a function of CaCO<sub>3</sub> granulometry and CMC structural properties.

For all calcite suspensions studied, ζ was negative and increased with a rise in DS for CMC Mw 2.5 x 10<sup>5</sup>. This means a higher amount of anionic charges in the medium, probably due to complete cationic calcite surface saturation by the

polymer, which was more effective with the increase in DS. When CMC with Mw 0.9 x 10<sup>5</sup> and DS 0.7 was used, different tendencies were observed, depending on the calcite employed. With an increase in calcite particle diameter, the negative ζ value became positive, probably due to incomplete saturation of the cationic calcite surface by CMC.

According to the zeta potential, good stability would be expected for all calcite suspensions, owing to the ionic charges on the surface. However, calcite particles with an anionic surface suggest CMC adsorption, which could lead to higher viscosities for the suspensions and the formation of low-permeability cakes during filtration. In this scenario, the formulation with the lowest negative zeta potential (F5) could lead to a more associative interaction between the particles and a more cohesive cake, resulting in high viscosity fluid and low filtrate volume, as depicted in Figures 3 and 6.

## 4. Conclusions

In this study, we investigated the effect of calcite particle size associated with CMC Mw and DS on the rheological and filtration properties of the aqueous suspensions, considering the general conditions used in drilling fluids. Zeta potential data were also used to clarify the interactions between calcite and CMC.

The higher Mw (2.5 x 10<sup>5</sup> g/mol) and lower DS (0.7) of CMC contributed to both higher viscosity and lower filtrate volume. This effect was improved in the presence of calcite, providing important evidence of CMC-CaCO<sub>3</sub> interactions. In addition, the use of a calcite sample with low average particle size but wide size distribution can contribute significantly to reducing filtrate loss across a porous medium. The zeta potential results provide even more evidence of the effective interactions between calcite and CMC. Lower negative zeta potential values were obtained for the suspensions containing higher CMC Mw (2.5 x 10<sup>5</sup> g/mol), lower DS CMC (0.7), and small calcite particle size. These results corroborate the rheological and filtration properties. In summary, the results of this paper indicate that the effectiveness of CMC-CaCO<sub>3</sub> (calcite) in the control of filtrate loss is related to good interaction between anionic groups of CMC and Lewis acid sites on the surface of the mineral and that this can be enhanced by proper selection of CMC and CaCO<sub>3</sub>.

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